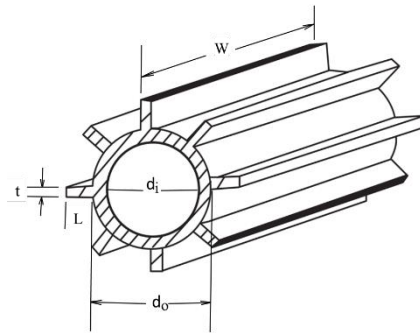


1-A steel tube ($k=60$ W/mK) of inner and outer diameters $D_i=20$ mm and $D_o=26$ mm, respectively, is used to transfer heat from hot gases flowing over the tube ($h_h=200$ W/m²K) to cold water flowing through the tube ($h_c=8000$ W/m²K). What is the cold-side overall heat transfer coefficient $U_{c=}$? To enhance heat transfer, 16 straight fins of rectangular profile are installed longitudinally along the outer surface of the tube. The fins are equally spaced around the circumference of the tube, each having a thickness of 2 mm and a length $L=20$ mm. Assume the pipe length to be 1 m. What is the corresponding overall heat transfer coefficient U_c ? [11.4] {Ans. $\eta_o=0.73$, $U_{no, fins}=249.1$ W/m².K, $U_{w, fins}=1306$ W/m².K }



2-The hot and cold inlet temperatures to a concentric tube heat exchanger are $T_{h,i}=200^\circ\text{C}$, $T_{c,i}=100^\circ\text{C}$, respectively. The outlet temperatures are $T_{h,o}=110^\circ\text{C}$ and $T_{c,o}=130^\circ\text{C}$. Is the heat exchanger operating in a parallel flow or in a counterflow configuration? What is the heat exchanger effectiveness? What is the NTU? Phase change does not occur in either fluid. [11.16] {Ans. $\epsilon=0.3$, NTU=0.377 }

3-A counterflow, concentric tube heat exchanger is designed to heat water from 20 to 80°C using hot oil, which is supplied to the annulus at 160°C and discharged at 140°C. The thin-walled inner tube has a diameter of $D_i=20$ mm, and the overall heat transfer coefficient is 450 W/m²K. The design condition calls for a total heat transfer rate of 3000 W.

(a) What is the length of the heat exchanger?

(b) After 3 years of operation, performance is degraded by fouling on the water side of the exchanger, and the water outlet temperature is only 65°C for the same fluid flow rates and inlet temperatures. What are the corresponding values of the heat transfer rate, the outlet temperature of the oil, the overall heat transfer coefficient, and the water-side fouling factor $R_{f,c}$? [11.18] {Ans. $L=1.08$ m, $U_{3y}=304.6$ W/m²K, $T_{ho}=145$ °C, $R_{fi} = 0.0010$ m².K/W }

4-Saturated process steam at 1 atm is condensed in a shell-and-tube heat exchanger (one shell, two tube passes). Cooling water enters the tubes at 15°C with an average velocity of 3.0 m/s. The tubes are thin walled and made of copper with a diameter of 14 mm and length of 0.5 m. The convective heat transfer coefficient for condensation on the outer surface of the tubes is 21,800 W/m² K.

(a) Find the number of tubes/pass required to condense 2.5 kg/s of steam.

(b) Find the outlet water temperature.

(c) Find the maximum possible condensation rate that could be achieved with this heat exchanger using the same water flow rate and inlet temperature [11.56] {Ans. $N_{tp}=223$ tubes, $N_t=446$ tubes, $T_{co}=28.2$ °C, $m_{cond,max}=16.14$ kg/s }

5-A shell-and-tube heat exchanger with one shell pass and 20 tube passes uses hot water on the tube side to heat oil on the shell side. The single copper tube has inner and outer diameters of 20 and 24 mm and a length per pass of 3 m. The water enters at 87°C and 0.3 kg/s and leaves at 27°C. Inlet and outlet temperatures of the oil are 7 and 37°C. What is the average convection coefficient for the tube outer surface? [11.58] {Ans. $\epsilon=0.75$, $h_i=4907$ W/m²K, $h_o=1246$ W/m²K }

6-A cross-flow heat exchanger consists of a bundle of 32 tubes in a 0.6-m² duct. Hot water at 150° C and a mean velocity of 0.5 m/s enters the tubes having inner and outer diameters of 10.2 and 12.5 mm. Atmospheric air at 10° C enters the exchanger with a volumetric flow rate of 1.2 m³/s. The convection heat transfer coefficient on the tube outer surfaces is 350 W/m² K. Assume the length of the tubes is 1 m. Estimate the fluid outlet temperatures [11.66] {Ans. $Re_i=25149$, $h_i=5280$ W/m²K, $U_o=323.7$ W/m²K, $\epsilon=0.235$, $T_{co}=32.6$ °C }